

Flow and Drying Simulation of Nanoparticle Suspension on Substrate

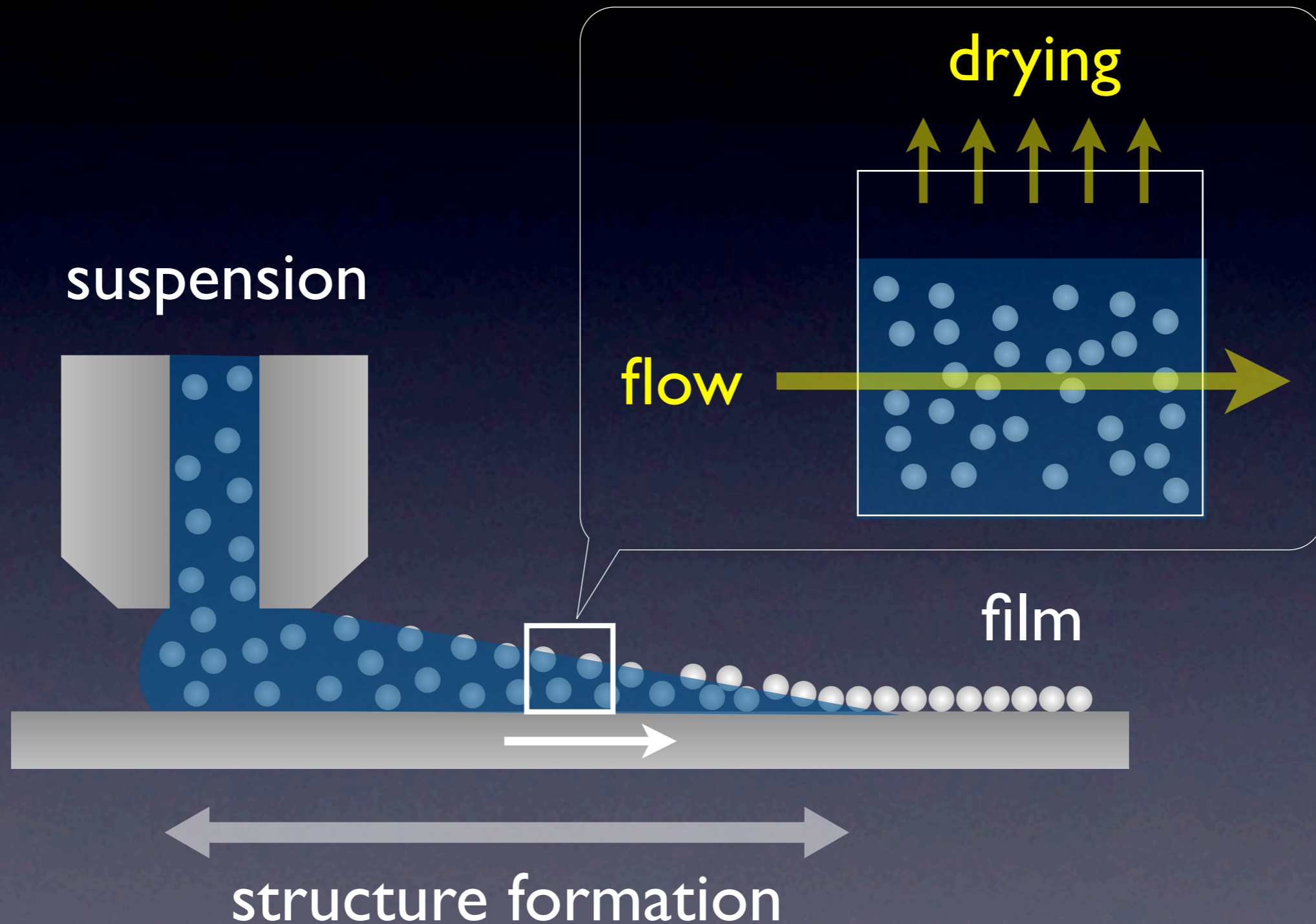
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Outline

- Continuous coating of nanoparticles suspension on substrate
- Direct simulation model for nanoparticles suspension in flow and drying
- Demonstration of present simulation model

Continuous coating on substrate



Peclét numbers for flow and drying

flow Peclét number

$$Pe_f = \frac{cd^2}{Dh}$$

drying Peclét number

$$Pe_d = \frac{eh}{D}$$

ratio of Peclét numbers

$$\frac{Pe_f}{Pe_d} = \frac{c}{e} \left(\frac{d}{h} \right)^2$$

$$\frac{Pe_f}{Pe_d} \sim 1$$




Both flow and drying influence structure formation

Objectives of this study

- Develop direct simulation model for nanoparticles suspension in flow and drying
- Perform flow and drying simulations of nanoparticles suspension on substrate
- Quantify structure formation of nanoparticles and evaluate effect of ratio of Peclet numbers

Direct simulation model

- Solves gas-liquid two phase flow on lattice using VOF method
- Solves translational motion and rotational motion of each particle
- Couples motion of particle with flow of solvent using fictitious domain method

 Interparticle hydrodynamic interaction is included without analytical model

Equations of fluid motion

fluctuating stress

$$\rho \frac{\partial \mathbf{v}}{\partial t} + \rho \mathbf{v} \cdot \nabla \mathbf{v} = -\nabla p + \nabla \cdot \mu \{ \nabla \mathbf{v} + (\nabla \mathbf{v})^T \} + \nabla \cdot \mathbf{S} + \rho \mathbf{g} + \Phi \alpha$$

acceleration

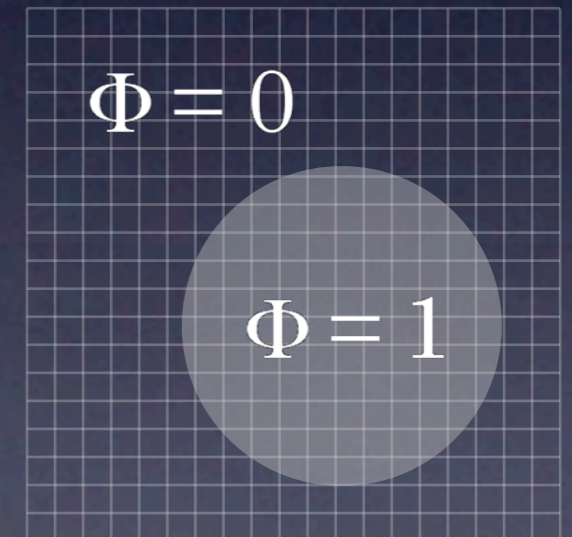
$$\alpha = \rho \frac{\mathbf{v}^p - \mathbf{v}}{\Delta t} + \rho \mathbf{v} \cdot \nabla \mathbf{v} + \nabla p - \nabla \cdot \mu \{ \nabla \mathbf{v} + (\nabla \mathbf{v})^T \} - \nabla \cdot \mathbf{S} - \rho \mathbf{g}$$

$$\rho = f \rho_1 + (1 - f) \rho_g, \quad \mu = f \mu_1 + (1 - f) \mu_g$$

VOF function

$$\frac{\partial f}{\partial t} + \mathbf{v} \cdot \nabla f + j = 0 \quad \nabla \cdot \mathbf{v} = \frac{\rho_1 - \rho_g}{\rho} j$$

evaporation rate



Equations of particle motion



$$m \frac{d\mathbf{v}}{dt} = \mathbf{F}^{\text{co}} + \mathbf{F}^{\text{D}} + \mathbf{F}^{\text{ca}} + \mathbf{F}^{\text{h}} + (\rho_p - \rho)V_p \mathbf{g}$$



$$I \frac{d\omega}{dt} = \mathbf{T}^{\text{co}} + \mathbf{T}^{\text{h}}$$

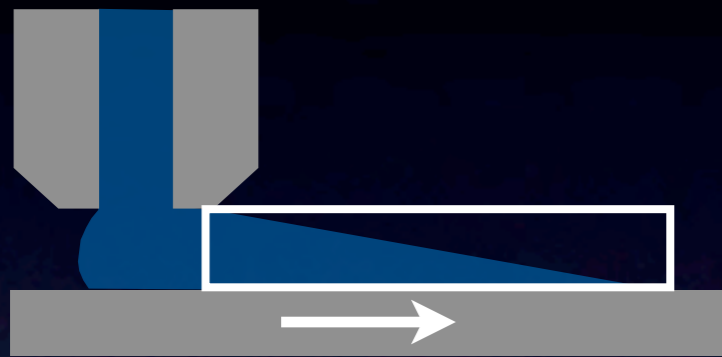
$$\mathbf{F}^{\text{h}} = - \int_{V_p} \rho \Phi \alpha \, d\mathbf{r}$$

acceleration

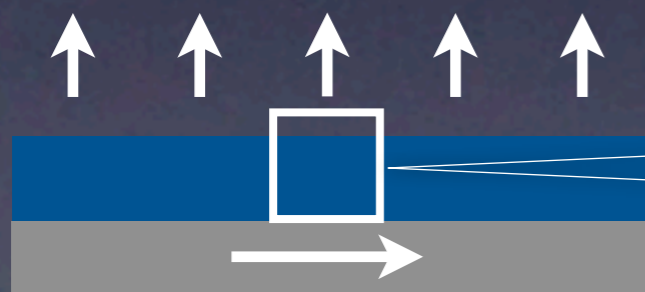
$$\mathbf{T}^{\text{h}} = - \int_{V_p} (\mathbf{r} \times \rho \Phi \alpha) \, d\mathbf{r}$$

acceleration

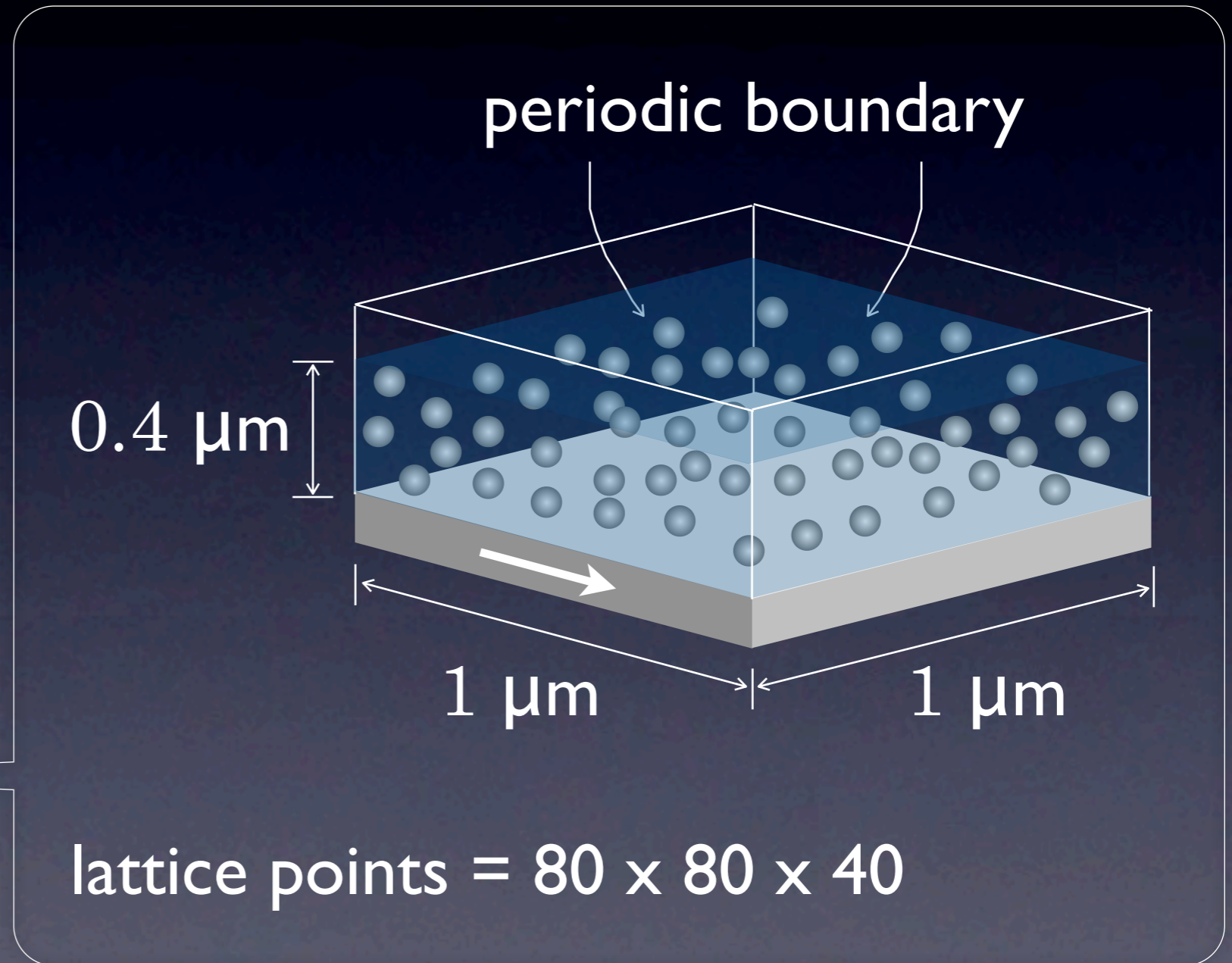
Simulation domain



drying



sliding substrate



Simulation conditions

concentrated repulsive system

- nanoparticles

$d = 0.1 \mu\text{m}$, $\phi_0 = 15 \text{ vol\%}$, $\zeta\text{-potential} = -50 \text{ mV}$

- solvent

water in normal temperature, $Pe_d = 930$

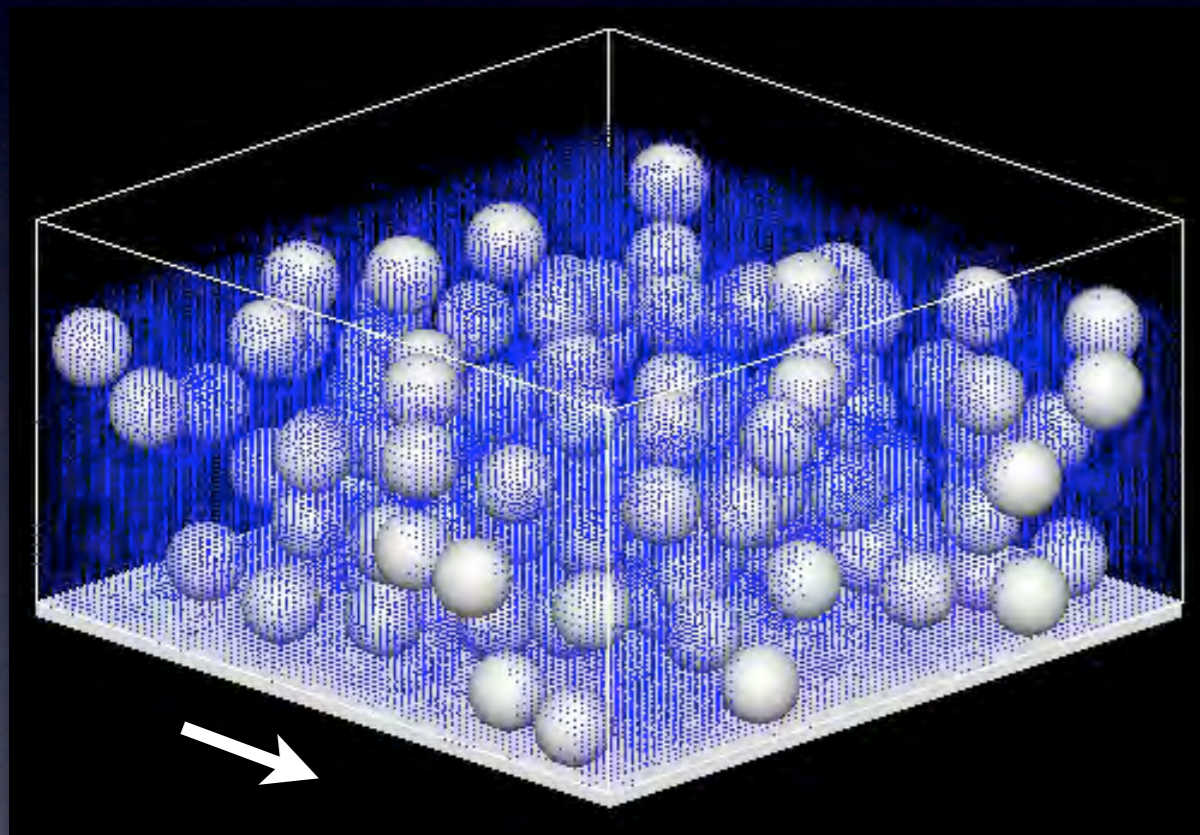
- sliding substrate

$\zeta\text{-potential} = -50 \text{ mV}$, $Pe_f = 93, 930$

➔ $Pe_f/Pe_d = 0.1, 1$

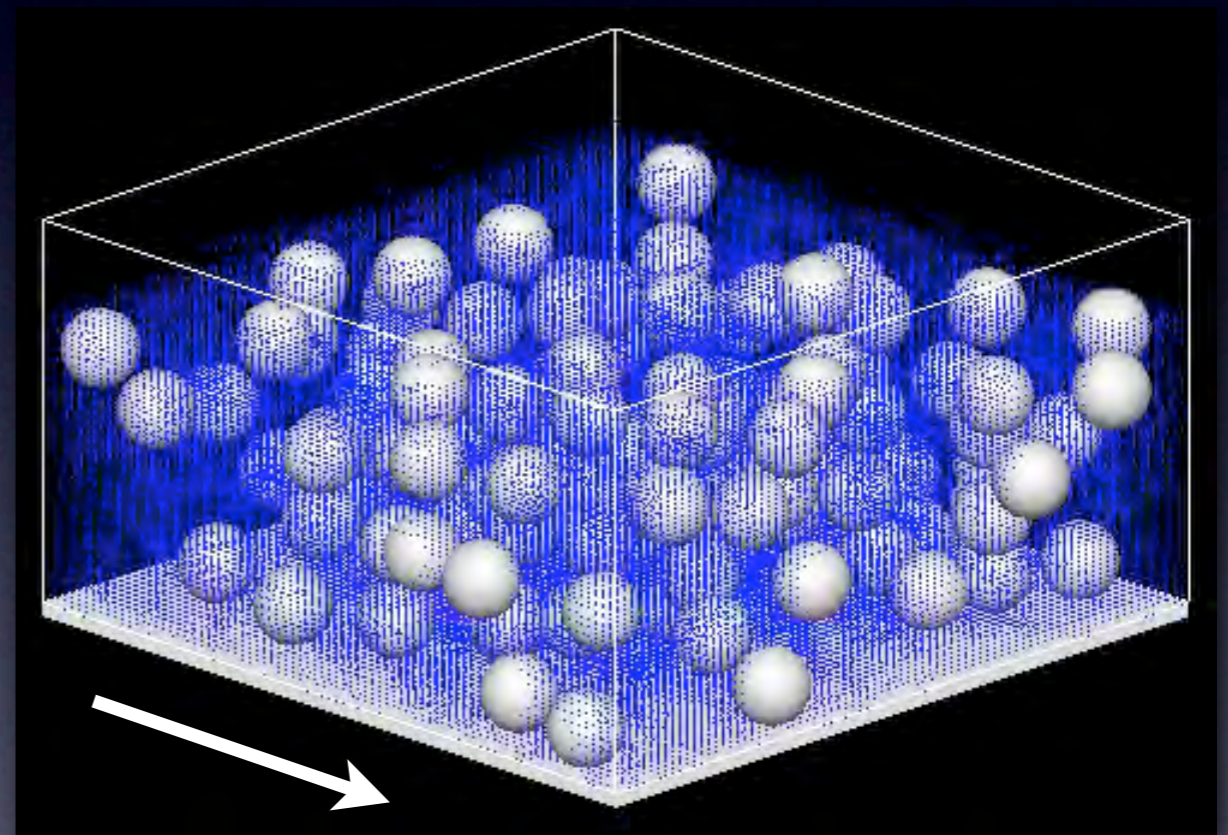
Simulation results

$$Pe_f/Pe_d = 0.1$$



low speed coating

$$Pe_f/Pe_d = 1$$



high speed coating

Quantification of structure formation

Non-dimensional Boundary Area (NBA)

$$\text{NBA} = \frac{\text{area of aggregates}}{\text{total area of particles}}$$

$$\text{NBA} = \frac{1}{12N} \sum_{k=0}^{12} \left\{ (12 - k)n(k) \right\}$$

k : coordinate number

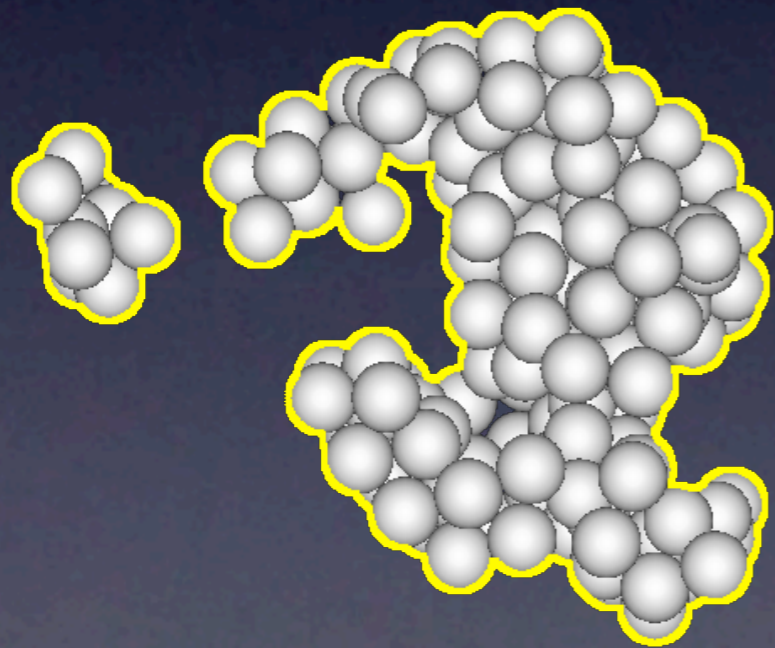
$n(k)$: number of particles with coordinate number of k

N : total number of particles



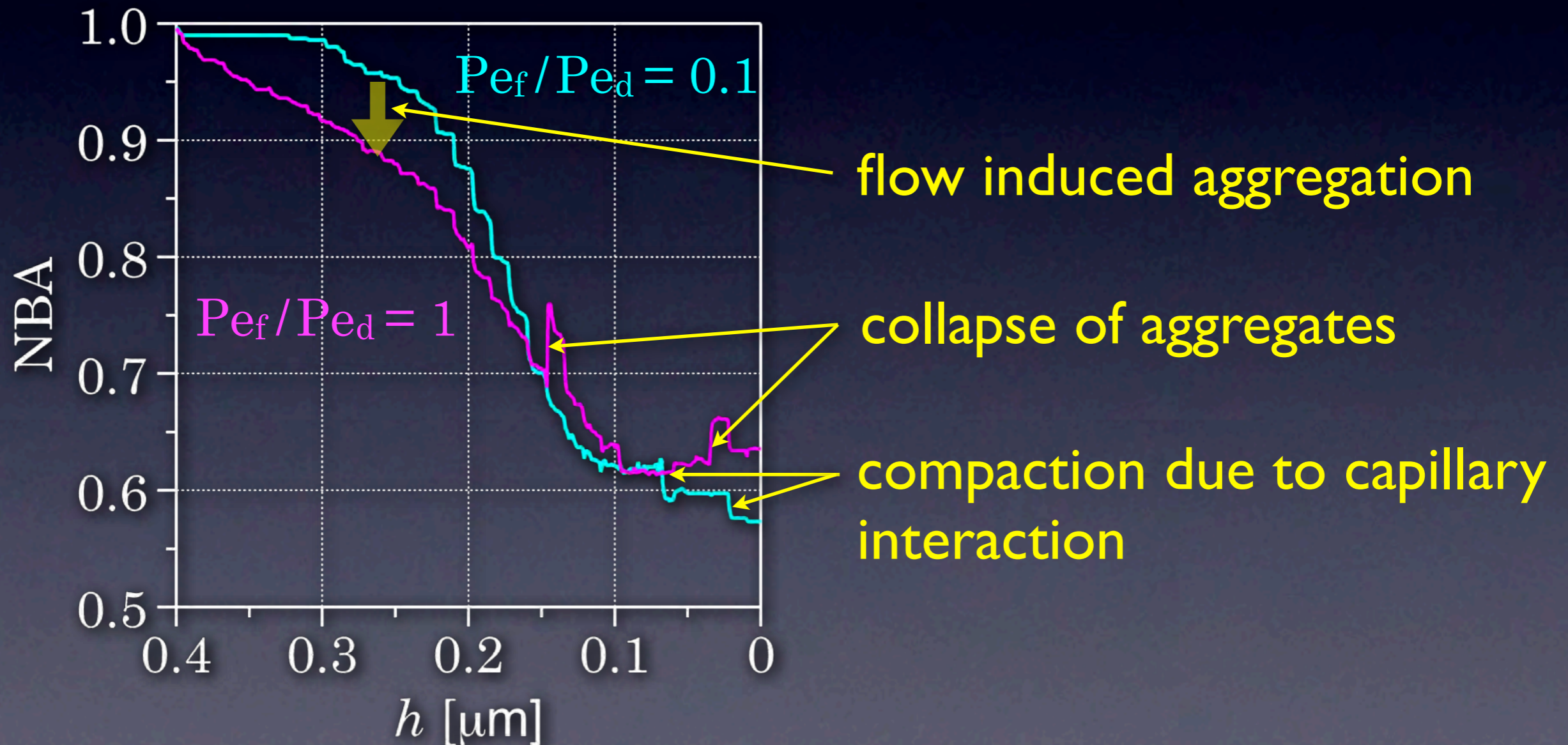
NBA = 0 : close-packed

NBA = 1 : dispersed



Effect of ratio of Peclet numbers

variation of NBA with thickness of wet film



Conclusion

- Developed direct simulation model for nanoparticles suspension in flow and drying
- Quantified structure formation of nanoparticles in flow and drying by use of NBA
- As ratio of Peclet numbers increases, compactness of final structure of nanoparticles decreases.